

**ENGINEERING SERVICES DEPARTMENT  
INSTRUMENT LOOP SPECIFICATION SHEET**



<b>Project</b>	NW PlasGas Demonstration Facility		<b>Unit Tag Number</b>	PCV1301B	
<b>Datasheet Document No.</b>	ENS-NWPVR-SPE-24006		<b>Revision</b>	1	
<b>Description</b>	Pressure regulator on the argon gas supply line to the Plasma Power Supply Y1401 in the NW PlasGas Demonstration Facility				
<b>Plant Location</b>	Necsa, Pelindaba, North-West Province.				
<b>Equipment Location</b>	NW PlasGas Demonstration Facility - Outside Laboratory 150, Building V-H2.				
<b>Safety Classification</b>	Non-classified(N) and SC-3(C)				
<b>Quality Classification</b>	Non-classified(N) and QC-3(C)				
<b>PROCESS CONDITIONS</b>	<b>UNITS</b>	<b>MINIMUM</b>	<b>NORMAL</b>	<b>MAXIMUM</b>	<b>ACCURACY</b>
<b>Measurement Range</b>	kPa(g)	400	600	1000	Medium
<b>Controlled Range</b>	kPa(g)	-	400	-	Medium
<b>GENERAL</b>	<b>MEASUREMENT POINT</b>			<b>CONTROL POINT</b>	
<b>Process Fluid</b>	Argon			Same as for measurement point	
<b>Fluid State</b>	Gas				
<b>P&amp;ID Number</b>	ENS-NWPVR-PID-24004 [6]				
<b>Line Number</b>	15-13-GAVP-10 [6]				
<b>Design Temperature [°C]</b>	98				
<b>Design Pressure [kPa(g)]</b>	24820				
<b>SIL Rating</b>	-				
<b>MEASUREMENT SPECIFICATION</b>					
<b>FLUID PROPERTIES</b>	<b>UNITS</b>	<b>MINIMUM</b>	<b>NORMAL</b>	<b>MAXIMUM</b>	<b>REFERENCE</b>
<b>Molecular Weight</b>	kg/kmol	-	39,948	-	Table 2-164 page 2-139 [1]
<b>Operating Temperature</b>	°C	-2.6	25	40	[2]
<b>Operating Pressure (upstream)</b>	kPa(g)	400	600	1000	Minimum from Page 6 [3] Normal from [5]
<b>Compressibility Factor</b>	Z	0,97	0,98	0,99	Fig A.9, page 278 [6]
<b>Density (@ min., normal, and max. for both operating pressure and temperature.)</b>	kg/m <sup>3</sup>	8,3	11,3	19,9	Note 1
<b>Viscosity (@ min., normal, and max. for operating temperature.)</b>	Pa.s	1,95E-05	2,75E-05	2,85E-05	Fig.2-32 page 2-321 [1]
<b>Specific Heat Ratio (Cp/Cv)</b>	-	-	1,67	-	Table 4.3, Page 165 [7]
<b>Thermal Conductivity</b>	W/m.K	0,01523	0,02148	0,02226	Note 2
<b>Required Measured Range (Upstream)</b>	kPa(g)	0	-	1500	-
<b>Required Measured Range (Downstream)</b>	kPa(g)	0	-	1500	-
<b>CONTROL INFORMATION</b>					
<b>VALVE SIZING INFO. &amp; SPECIFICATION</b>	<b>UNITS</b>	<b>MINIMUM</b>	<b>NORMAL</b>	<b>MAXIMUM</b>	<b>REFERENCE</b>
<b>Valve Inlet Pressure</b>	kPa(g)	400	600	1000	Minimum from Page 6 [3] Normal from [5]
<b>Valve Outlet Pressure = Regulator Setpoint Pressure</b>	kPa(g)	-	400	-	[5]
<b>Maximum Differential Pressure Allowed Across Control Valve</b>	kPa	-	-	600	-
<b>Critical Flow</b>	-	-	No	-	-
<b>Mass Flowrate</b>	kg/h	0	3	10	Page 6 [3]
<b>P<sub>c</sub> - Critical Pressure</b>	kPa(a)	-	4900	-	Table 2-164 page 2-139 [1]
<b>Fail Action</b>	-	N/A			-
<b>Seat Leakage Class</b>	Supplier to advise				-
<b>Maximum Shut - Off Differential Pressure</b>	kPa(g)	1000			-
<b>VALVE MECHANICAL PROPERTIES</b>					
<b>MATERIAL OF CONSTRUCTION</b>					
<b>Body</b>	<b>Bellows</b>	<b>Spring</b>		<b>Seat</b>	<b>Disk and STEM</b>
316 Stainless Steel	Supplier To advise	NA		Die-Formed Flexible Graphite With Anti-Extrusion Rings	Stainless Steel
<b>Bonnet/Cap</b>		<b>Type</b>		<b>Wetted parts</b>	<b>Non-wetted parts</b>
316 Stainless Steel		Two-stage		Stainless Steel	Stainless Steel
<b>PROCESS CONNECTION</b>					
	<b>Flange Spec.</b>		<b>Flange Rating</b>		<b>Pipe Size (NB)</b>
<b>Inlet</b>	SS, ASTM A182-F316/316L, ASME B16.5 (Supplier To Advise on Alternatives)		Class 3000		15
<b>Outlet</b>	SS, ASTM A182-F316/316L, ASME B16.5 (Supplier To Advise on Alternatives)		Class 3000		15
<b>Valve rating</b>	Class 3000				
<b>ALARM / SWITCH</b>	<b>FALLING</b>		<b>RISING</b>		<b>UNITS or %</b>
	<b>Low Low</b>	<b>Low</b>	<b>High</b>	<b>High High</b>	
<b>LOCAL ALARM</b>	-	-	-	-	-
<b>REMOTE ALARM</b>	-	-	-	-	-
<b>SWITCH ONLY</b>	-	-	-	-	-
<b>DISPLAY</b>	<b>LOCAL</b>		<b>REMOTE</b>		<b>RECORDING</b>
	Yes		-		-
<b>REFERENCE DRAWINGS / DOCUMENTS</b>					
[1] Perry, R. H., & Green, D. W. (1997). Perry's Chemical Engineers Handbook 7th Edition. McGraw-Hill Company.					
[2] SHEQ-2011-REP-01017,2011: Pelindaba Site, Site Description Rev 2, NECSA					
[3] ENS-NWPVR-CLC-24013, Process Gases Requirements for the NW PlasGas Demonstration System					
[4] Sinnott, R. K. (2005). Coulson & Richardson's CHEMICAL ENGINEERING, Chemical Engineering Design, Volume 6, 4th Edition.					
[5] ENS-NWPVR-PID-24004, NW PlasGas Demonstration Plant P&ID Diagram, Subsystem 13					
[6] Rase, H. F. (1963). Piping Design for Process Plant. New York: John Wiley & Sons, Inc.					
[7] Joseph F. Louvar, Daniel A Crowl, 2011: Chemical Process Safety Fundamentals with Applications, 3rd edition					

**NOTES**

1) Minimum density was calculated from the highest temperature and lowest pressure, normal density at normal conditions, and maximum density at the lowest temperature and highest pressure

2) Thermal conductivity was calculated from Equation 8.13 on Section 8.8.3 page 321 [4]. The specific heat capacity used in the equation was calculated from Equation on Appendix C, Page 939 of [4] at minimum, normal and maximum temperature.

	<b>Name</b>	<b>Signature</b>	<b>Date</b>
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