ENGINEERING SERVICES DEPARTMENT



SCRUBBER S1501 SPECIFICATION SHEET

Project	NW PlasGas Project	Unit Tag Number	S1501	
Datasheet Document No.	ENS-NWPVR-SPE-24020	Revision	R2,0	
Description	Shared KOH Scrubber for the Low-Level Waste Plasma Gasification (NW PlasGas) and the Uranium Contaminated Waste Oil Plasma Gasification (CWOPG) Demonstration Facilities			
Plant	Merged NW PlasGas and CWOPG Facilities			
Plant Location	Building V-H2, Laboratory 150 (scrubber housed inside a secondary enclosure Y1410)			
Safety Classification	SC-2(C) and SC-3(N)			
Quality Classification	QC-2(C) and QC-3(N)			
FLUID PROPERTY DATA				

FLUID PROPERTY DATA							
			NW PLASGAS			CWOPG	
		UNITS	GAS	LIQUID FROM QUENCH	LIQUID FROM RECYCLE	GAS	SCRUBBING LIQUID
Fluid Deceription			CO ₂ , HCI, H ₂ O, O ₂ ,			CO ₂ , HCl, HF, H ₂ O, O ₂ ,	H ₂ O, KOH, KF, KCI,
Fluid Description			N ₂ Note 1	KHCC) ₃ Note 2	N ₂ Note 3	K ₂ CO ₃ , KHCO ₃ Note 4
Density (at average temperature) kg/m³		kg/m ³	0,893	1274,8		0,833	1274,8
Viscosity		сР	0,02	1,6		0,02	1,6
Operating	Minimum	°C	25	2	25	25	25
	Normal inlet	°C	80	75	35	90	35
Temperature	Normal outlet	°C	35	56,1 (Cd	ombined)	35	49,53
	Maximum	°C	80	8	30	90	80
Flow rate (feed to	the scrubber) Note	kg/h	58,66	1013	2960	57,92	4429
6		m ³ /h Note 5	44,14	0,79	3,58	45,39	5,02
0	Minimum	kPa(a)	77	77	317,7	77	413,0 Note 8
Operating Pressure	Normal	kPa(a)	82	82	320,1	171	416,1 Note 8
Fiessule	Maximum	kPa(a)	87	87	337,5	200	438,8 Note 8
Permissable pressure drop over packed bed kPa		1,5					
Design pressure drop over packed kPa			Supplier to advise				
Design temperature °C		90					
Design pressure kPa(a)		750					
			CAPACI	TY DATA			
Column diameter				6 mm, base	d on a 355 m	m Polypropylene pipe	
Bed height			2 m				
Type of packing			Pall rings				
Packing material			Polypropylene				
Packing size			16 mm				
Sump volume			2 m ³				
Sump dimension	S		Supplier to advise				
Instrumentation	rumentation Ultra guided radar level indicator transmitter on the scrubber sump, more informati available in the purchase specification			ore information			
Accessories			Liquid redistribution every 1.45 m (maximum); supplier to advise optimal position				
			Demister inside scrubber between top of packed bed and en gas outlet				
			Spray nozzles above packed bed for introduction of recycled scrubbing liquid				
		Liquid distribution manifold for proper distribution of scrubbing liquid through the diameter of the packed column.					
		Packing support					
Operating hours 6 hours per day, plus 1 hour for startup and 1 hour for shutdown, 5 days per week			ys per week				
MECHANICAL SECTION							
Process exposed material Polypropylene (scrubber sump and column)							
Process connections Note 7 Flanged (150			Flanged (150 lb rate	ed), details a	vailable in Ρι	rchase specification doc	ument

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SITE CONDITIONS			
Altitude	m	1300	
Site location		Pelindaba East, H-Building	
Atmospheric Pressure (min./max.)	kPa(a)	Min: 87,4; Max: 88,3	
Ambient Temperature (min./max.)	°C	Min: 2; Max: 32	

REFERENCE DRAWINGS AND DOCUMENTS

- [1] ENS-NWPVR-CLC-24015: Scrubber Design for the Low-Level Waste Plasma Gasification (NW PlasGas) Demonstration System
- [2] ENS-OWPVR-CLC-24006: Scrubber Design for the Uranium Contaminated Waste Oil Plasma Gasification Project
- [3] ENS-NWPVR-PID-24002: P&ID Diagram: NW PlasGas Demonstration Plant Subsystem 15
- [4] ENS-NWPVR-SPE-24019: Purchase Specification for the Wet Scrubber in the Combined NW PlasGas/Waste Oil Demonstration Facility

NOTES

- Note 1: For the PlasGas Facility, the composition of the gas entering the scrubber is (w/w): 56.97% CO₂, 2.98% HCl, 18.82% H₂O, 11.17% O₂, and 10.06% N₂. The stream will include 1013 kg/h scrubbing liquid used for quenching purposes with the composition of Note 2.
- Note 2: For the PlasGas Facility, the scubber solution composition will change over time due to the chemical reactions taking place in the scrubber. At the end of phase 1, the composition (w/w) will be 67.67% water, 1.05% KCl, and 30.78% K₂CO₃. At the end of phase 2, the composition will be 58.87% water, 1.79% KCl, and 38.04% KHCO₃. At the end of the final phase, the composition will be 62.52% water, 4.26% KCl, and 31.20% KHCO₃.
- Note 3: For the CWOPG Facility, the composition of the gas entering the scrubber is (w/w): 53.68% CO₂, 0.04% HCl, 0.01% HF, 0.01
- Note 4: For the CWOPG Facility, the scubber solution composition will change over time due to the chemical reactions taking place in the scrubber. At the end of phase 1, the composition (w/w) will be 67.22% water, 0.014% KCI, 0.004% KF, and 32.76% K $_2$ CO $_3$. At the end of phase 2, the composition will be 60.22% water, 0.024% KCI, 0.007% KF, and 39.75% KHCO $_3$. At the end of the final phase, the composition will be 65.34% water, 0.061% KCI, 0.016% KF, and 34.5814% KHCO $_3$.
- Note 5: Gas flow rate given at normal conditions: 20°C and 101.325 kPa
- Note 6: Gas entering the scrubber may be two-phase flow, since reactions will already be taking place in the quench (NW PlasGas) and the liquid ring pump (CWOPG).
- Note 7: Detailed information on number and position of connections available in the Purchase Specification, Table 8
- Note 8: Estimated pressure since pump has not yet been sized

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