


ENGINEERING SERVICES DEPARTMENT						 <small>national e-learning centre of south africa</small> <small>national e-learning centre of south africa</small>	
INSTRUMENT LOOP SPECIFICATION SHEET							
Project	PTFE Filter Destruction Project			Unit Tag Number	PCV83343B		
Datasheet Document No.	ENS-FDP-SPE-24043			Revision	1		
Description	Pressure regulator on the argon gas supply line to the Plasma Power Supply Y82016 in the PTFE Filter Destruction Facility						
Plant Location	Necsa, Pelindaba, North-West Province.						
Equipment Location	PTFE Filter Destruction Facility - Outside Laboratory 131, Building V-H2.						
Safety Classification	Non-classified(N) and SC-3(C)						
Quality Classification	Non-classified(N) and QC-3(C)						
PROCESS CONDITIONS	UNITS	MINIMUM	NORMAL	MAXIMUM	ACCURACY		
Measurement Range	kPa(g)	450	600	1000	Medium		
Controlled Range	kPa(g)	-	400	-	Medium		
GENERAL	MEASUREMENT POINT			CONTROL POINT			
Process Fluid	Argon			Same as for measurement point			
Fluid State	Gas						
P&ID Number	ENS-FDP-PID-24005 [6]						
Line Number	15-833-GAVP-062						
Design Temperature [°C]	93						
Design Pressure [kPa(g)]	21340						
SIL Rating	-						
MEASUREMENT SPECIFICATION							
FLUID PROPERTIES	UNITS	MINIMUM	NORMAL	MAXIMUM	REFERENCE		
Molecular Weight	kg/kmol	-	39,948	-	Table 2-164 page 2-139 [1]		
Operating Temperature	°C	-2.6	25	40	[2]		
Operating Pressure (upstream)	kPa(g)	450	600	1000	Minimum (Section 4.2.3 [3]).		
Compressibility Factor	Z	0,97	0,98	0,99	Fig A.9, page 278 [7]		
Density (@ min., normal, and max. for both operating pressure and temperature.)	kg/m³	8,3	11,3	19,9	Note 1		
Viscosity (@ min., normal, and max. for operating temperature.)	Pa.s	1,95E-05	2,75E-05	2,85E-05	Fig.2-32 page 2-321 [1]		
Specific Heat Ratio (Cp/Cv)	-	-	1,67	-	Table 4.3, Page 165 [8]		
Thermal Conductivity	W/m.K	0,01523	0,02148	0,02226	Note 2		
Required Measured Range (Upstream)	kPa(g)	0	-	1500	Page 11 [4]		
Required Measured Range (Downstream)	kPa(g)	0	-	1500	Page 11 [4]		
CONTROL INFORMATION							
VALVE SIZING INFO. & SPECIFICATION	UNITS	MINIMUM	NORMAL	MAXIMUM	REFERENCE		
Valve Inlet Pressure	kPa(g)	450	600	1000	Minimum (Section 4.2.3 [3]).		
Valve Outlet Pressure = Regulator Setpoint Pressure	kPa(g)	-	400	-	[6]		
Maximum Differential Pressure Allowed Across Control Valve	kPa	-	-	600	-		
Critical Flow	-	-	No	-	-		
Mass Flowrate	kg/h	0	3	10	Page 11 [4]		
P _c - Critical Pressure	kPa(a)	-	4900	-	Table 2-164 page 2-139 [1]		
Fail Action	-	N/A			-		
Seat Leakage Class	-	Supplier to advise			-		
Maximum Shut - Off Differential Pressure	kPa(g)	1000			-		
VALVE MECHANICAL PROPERTIES							
MATERIAL OF CONSTRUCTION							
Body	Bellows	Spring		Seat		Disk and STEM	
316 SS	Supplier to advise	NA		Die-formed flexible graphite with anti-extrusion rings		316 SS	
Bonnet/Cap		Type		Wetted parts		Non-wetted parts	
316 SS		Two-stage		SS		SS	
PROCESS CONNECTION							
	Flange Spec.			Flange Rating		Pipe Size (NB)	
Inlet	SS, ASTM A182-F316/316L, ASME B16.5 (Supplier shall advise of alternatives)			Class 3000		15	
Outlet	SS, ASTM A182-F316/316L, ASME B16.5 (Supplier shall advise of alternatives)			Class 3000		15	
Valve rating	Class 3000						
ALARM / SWITCH	FALLING		RISING		UNITS or %	INTERLOCKS	
	LowLow	Low	High	High High			
LOCAL ALARM	-	-	-	-	-	N/A	
REMOTE ALARM	-	-	-	-	-		
SWITCH ONLY	-	-	-	-	-		
DISPLAY	LOCAL			REMOTE		RECORDING	
	Yes			-		-	
REFERENCE DRAWINGS / DOCUMENTS							
[1] Perry, R. H., & Green, D. W. (1997). Perry's Chemical Engineers Handbook 7th Edition. McGraw-Hill Company.							
[2] SHEQ-2011-REP-01017,2011: Pelindaba Site, Site Description Rev 2, NECSA							
[3] ENS-FDP-CLC-24014, Mass Balance Calculation for the PTFE Filter Destruction System							
[4] ENS-FDP-LST-24003, PTFE Filter Destruction Plant Instrumentation List							
[5] Sinnott, R. K. (2005). Coulson & Richardson's CHEMICAL ENGINEERING, Chemical Engineering Design, Volume 6, 4th Edition.							
[6] ENS-FDP-PID-24004, PTFE Filter Destruction Project - P&ID Diagram: Gas Supply System 833							
[7] Rase, H. F. (1963). Piping Design for Process Plant. New York: John Wiley & Sons, Inc.							
[8] Joseph F. Louvar, Daniel A Crowl, 2011: Chemical Process Safety Fundamentals with Applications, 3rd edition							

NOTES			
1) Minimum density was calculated from the highest temperature and lowest pressure, normal density at normal conditions, and maximum density at the lowest temperature and highest pressure			
2) Thermal conductivity was calculated from Equation 8.13 on Section 8.8.3 page 321 [5]. The specific heat capacity used in the equation was calculated from Equation on Appendix C, Page 939 of [5] at minimum, normal and maximum temperature.			
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